

## Assessment of Chemical Solvent Processing of Sour Natural Gas to Meet Sales Gas Quality

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### ABSTRACT

The growing demand for environmentally friendly natural gas that meets market standards highlights the necessity for effective treatment processes. High concentrations of acid gases, such as H<sub>2</sub>S and CO<sub>2</sub>, in natural gas streams pose safety and environmental risks. As the energy landscape evolves, investing in innovative solutions to address these challenges becomes essential for the industry. This study aims to assess the performance and economic viability of chemical solvent-based sweetening techniques in treating sour natural gas. Objectives include evaluating how these methods can effectively reduce the levels of acid gases with stringent pipeline sales gas specifications. Factors such as environmental impact, efficiency of the sweetening process, and the overall lifecycle costs associated with the implementation of these chemical solvent technologies are considered. The focus is a comparison of the absorption efficiency, regeneration energy requirements, and solvent degradation rates of widely used amine-based systems, specifically MEA, DEA, and MDEA. With a range of operating conditions, including variations in temperature, pressure, and CO<sub>2</sub> concentration. Identify the performance characteristics of each amine in terms of their ability to capture carbon dioxide effectively, the energy costs associated with regenerating the amine solvents after absorption, and the rates at which these solvents degrade over time. The method of carrying out this work includes the collection of field data, and advanced simulation models were utilized to analyze the solvent performance on the efficiency of (H<sub>2</sub>S) and (CO<sub>2</sub>) removal. The results indicate that blending MDEA (Methyldiethanolamine) with piperazine (PZ) promoters enhances the efficiency of acid gas removal processes. The results show a reduction in corrosion potential; the treated gas meets stringent international sales gas specifications, achieving H<sub>2</sub>S concentrations of less than 4 parts per million (ppm) and CO<sub>2</sub> levels below 2%. Conclusively, this level of performance meets regulatory standards and ensures the overall quality of the processed gas, making it more suitable for market applications.

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## 1. Introduction

Natural gas is gaining recognition as a crucial transitional energy source, primarily due to its significantly lower carbon intensity when compared to other fossil fuels like coal and oil. These characteristics position natural gas as a more environmentally friendly option in the quest to reduce greenhouse gas emissions and combat climate change. As countries shift toward cleaner energy solutions, natural gas serves as a bridge, facilitating the move away from more polluting energy sources while supporting the transition to renewable energy alternatives. Its role in this energy evolution is becoming increasingly vital in global energy strategies. A substantial portion of the natural gas produced around the world is classified as sour gas. This type of gas contains a range of undesirable acid gases, notably hydrogen sulfide (H<sub>2</sub>S) and carbon dioxide (CO<sub>2</sub>). These impurities not only pose challenges for processing and transportation but also require careful handling due to their toxicity and environmental impact[1]. As a result, sour gas must undergo extensive treatment to remove these harmful components before it can be safely utilized or transported to market. The presence of these impurities in the gas is a significant concern, as they not only introduce serious risks related to corrosion of pipeline infrastructure but also pose potential health hazards to individuals and environmental threats to

surrounding ecosystems. Furthermore, these contaminants can compromise the integrity and purity of the gas, making it non-compliant with both pipeline regulations and the specifications required by end users. This non-compliance can lead to operational inefficiencies, increased maintenance costs, and potential legal repercussions, ultimately highlighting the critical need for stringent quality control measures throughout the gas supply chain. To comply with rigorous sales gas quality standards, which generally mandate hydrogen sulfide (H<sub>2</sub>S) concentrations to be kept below 4 parts per million (ppm) and carbon dioxide (CO<sub>2</sub>) levels under 2 percent, sour gas needs to undergo a highly effective sweetening process. This vital treatment not only removes harmful impurities but also ensures that the gas meets the required specifications for safe and efficient utilization in various applications.

The use of chemical solvent processing stands out as one of the most prevalent and efficient technologies for the removal of acid gases. This method leverages specific chemical solvents to selectively absorb and eliminate harmful gaseous contaminants, thereby ensuring cleaner emissions and improved air quality. Its widespread adoption in various industrial applications underscores its reliability and effectiveness in tackling the challenges posed by acid gas pollution. This method primarily utilizes a range of

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alkanolamine-based solvents, which are essential for effective gas treatment processes. Key examples include monoethanolamine (MEA), a widely used solvent known for its strong absorption properties and efficiency in removing acid gases like carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S) from natural gas. Diethanolamine (DEA) is another important solvent that offers enhanced performance in certain applications, particularly in sweetening natural gas. Additionally, diglycolamine (DGA) provides a more selective absorption process, making it valuable for operations requiring the removal of CO<sub>2</sub> without significant loss of methane. Another notable solvent is methyldiethanolamine (MDEA), which has gained popularity due to its lower regeneration energy requirements and effectiveness in treating gases with low acid content. Furthermore, proprietary blends such as Adip have been developed to optimize performance and tailor specific solutions to meet unique operational requirements in industrial gas processing. Collectively, these alkanolamine-based solvents play a crucial role in achieving efficient and effective purification of gas streams. These solvents function through reversible absorption mechanisms, effectively capturing acid gases in the contactor column. During this process, the solvent selectively binds with the gases, allowing for efficient separation. Once the absorption phase

is complete, the attached gases are released during the regeneration stage, ensuring that the solvent can be reused for repeated cycles of absorption and desorption. This sophisticated process allows for optimized removal of harmful acid gases, contributing to cleaner industrial practices. MEA, or Monoethanolamine, is a widely used solvent in gas treatment processes due to its high reactivity with carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S). This property allows MEA to effectively capture and remove these gases from industrial emissions, contributing to cleaner air and reduced environmental impact. However, despite its excellent removal efficiency, the use of MEA is associated with significant drawbacks. One major concern is its high energy demand during regeneration, which requires substantial heat input to separate the absorbed gases from the solvent. Additionally, MEA is prone to degradation over time, particularly when exposed to high temperatures and contaminants, leading to a decrease in its effectiveness and necessitating frequent replacement. Addressing these challenges is essential for optimizing the use of MEA in gas treatment applications while minimizing operational costs and environmental risks. In contrast, MDEA (methyldiethanolamine) offers a highly efficient and selective method for removing carbon dioxide (CO<sub>2</sub>) from gas streams, showcasing significantly lower energy demands

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compared to other solvents. This efficiency is further enhanced when MDEA is combined with activators such as piperazine, which optimizes its performance and facilitates a more effective capture of CO<sub>2</sub>, making it an ideal choice for various industrial applications. Apart from alkanolamines, a variety of alkaline salt solutions are employed in various processes, most notably those such as Hot Pot, Catacarb, and the Benfield process. These solutions, particularly potassium carbonate-based ones, are essential for capturing carbon dioxide effectively in environments where high volumes of gas need to be treated or where elevated temperatures are a factor. The Hot Pot system, for example, optimizes heat exchange to enhance efficiency, while Catacarb leverages the unique properties of the carbonate salts to achieve significant CO<sub>2</sub> absorption rates. Similarly, the Benfield process is renowned for its ability to operate under challenging conditions, making it a preferred choice in industries that demand reliable performance in gas treatment applications. These advanced alkaline solutions provide not only efficiency in capture but also flexibility and adaptability to a wide range of operational environments. These advanced solutions demonstrate significant advantages, particularly in their exceptional thermal stability and minimized solvent losses. These characteristics make them highly effective for large-scale CO<sub>2</sub> removal in

integrated gas processing facilities, ensuring efficient operation and environmental sustainability[2].

This study provides a comprehensive examination of the performance and efficiency of various chemical solvent systems used in treating sour natural gas, with a specific focus on achieving pipeline-quality standards. It explores the intricacies of the treatment process, including the optimization techniques employed to enhance solvent effectiveness and minimize operational costs. Additionally, the research delves into the economic implications of adopting these solvent systems, analyzing their cost-effectiveness, scalability, and potential impact on the natural gas industry. Through this analysis, the study aims to identify best practices and innovative approaches that could lead to improved environmental outcomes and greater sustainability in natural gas processing. This study seeks to establish a comprehensive framework for selecting the most suitable sweetening technology tailored to specific field conditions. By thoroughly evaluating key factors such as absorption efficiency, which measures the effectiveness of the technology in removing unwanted compounds; regeneration energy, which assesses the energy required to restore the solvent for reuse; and solvent durability, which considers the lifespan and stability of the solvent under operational conditions, we aim to provide detailed insights.

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This approach will help identify the best sweetening solutions that not only enhance operational efficiency but also align with environmental and economic sustainability goals[13].

## 2. Literature review

The processing of sour natural gas, which contains significant amounts of hydrogen sulfide and carbon dioxide, is an essential operation within the natural gas industry. This process is crucial for ensuring that the gas meets stringent sales gas quality standards, enabling it to be safely transported and utilized as a reliable energy source. Effective treatment of sour gas involves several steps, including the removal of impurities and contaminants through various technologies such as amine gas treating and membrane separation[3]. By thoroughly refining sour natural gas, operators can enhance its quality, minimize environmental impact, and ensure compliance with regulatory requirements, ultimately providing a dependable product for consumers and industries alike. Chemical solvent processes have become a focal point of research and application in the field of gas treatment, especially for their effectiveness in removing acid gases like carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S). Among the various methods, the use of alkanolaminesuch as monoethanolamine (MEA),

diethanolamine (DEA), and triethanolamine (TEA)alongside alkaline salt solutions has garnered significant attention. These compounds work through a process of chemical absorption, where the alkanolamines react with the acidic gases to form soluble amine salts, facilitating their removal from industrial emissions. Furthermore, the selection of the appropriate solvent depends on several factors, including the specific gas composition, temperature, pressure, and the desired purity levels of the treated gas. In practice, optimizing these processes can enhance efficiency, reduce operational costs, and ensure compliance with environmental regulations. Enhanced solvent formulations and innovative process designs continue to be a subject of extensive research, aiming to improve the overall performance and sustainability of acid gas removal techniques. Alkanolamines like monoethanolamine (MEA), diethanolamine (DEA), diglycolamine (DGA), methyldiethanolamine (MDEA), and proprietary blends such as Adip are commonly employed due to their high reactivity with acid gases.[11].

Alkanolamines, including monoethanolamine (MEA), diethanolamine (DEA), diglycolamine (DGA), and methyldiethanolamine (MDEA), play a crucial role in industrial processes, particularly in gas treatment applications. These compounds are valued for their high

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reactivity with acid gases, such as carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S), which are often present in natural gas and refinery streams. MEA is typically utilized for its effectiveness in removing CO<sub>2</sub> from gas streams, making it a popular choice in the natural gas processing and petrochemical industries. DEA offers a balance between absorption rate and regeneration efficiency, making it suitable for various applications, including gas processing and wastewater treatment. DGA, on the other hand, is known for its enhanced performance in conditions of high concentration of acid gases, providing superior absorption and lower volatility. MDEA is favored for its ability to selectively absorb H<sub>2</sub>S while minimizing CO<sub>2</sub> absorption, which is particularly beneficial in specific refining contexts[4]. Additionally, proprietary blends such as Adip combine these alkanolamines to optimize their performance, tailoring them for specific operational needs. These blends can enhance absorption rates, reduce solvent loss, and improve overall process efficiency, making them an essential tool in managing operational costs and environmental compliance. In summary, the selection of alkanolamines is critical for effective acid gas removal, with each compound offering unique advantages depending on the application and operating conditions.

MEA (Monoethanolamine) is classified as a primary amine known for its quick reaction kinetics, making it effective in various chemical processes, particularly in capturing carbon dioxide from flue gases. However, its use is accompanied by significant challenges, including high energy demands for the regeneration process. This regeneration is necessary to restore the amine's absorption capacity after it has reacted with carbon dioxide. Additionally, MEA is prone to solvent degradation, which can lead to the formation of byproducts that not only lessen its effectiveness over time but may also introduce complications in downstream processing. The balance between its rapid reactivity and the associated high operational costs poses a critical consideration for industries utilizing MEA in carbon capture and other applications[5]. DEA (Diethanolamine) and DGA (Diglycolamine) are known for their moderate reaction rates, which allow for efficient gas treatment processes without excessive energy costs. Additionally, both substances exhibit improved stability under various operational conditions, making them reliable choices for applications such as carbon capture and gas purification. On the other hand, MDEA (Methyldiethanolamine), being a tertiary amine, presents distinct advantages in terms of energy efficiency. It requires lower energy consumption during the regeneration phase, allowing for cost-effective recovery of the amine solution.

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However, one of MDEA's drawbacks is its slower absorption rates compared to DEA and DGA. This means that while MDEA may save energy during regeneration, the overall performance in terms of gas absorption may be less efficient, necessitating careful consideration of the specific requirements of the gas treatment application when selecting the appropriate amine[17].

Recent studies have demonstrated that blending methyl diethanolamine (MDEA) with activators such as piperazine significantly improves absorption rates in various applications, particularly in carbon dioxide capture processes. This combination not only enhances the effectiveness of the absorption but also ensures that energy efficiency is maintained throughout the operation. The incorporation of piperazine acts to increase the reactivity of the solvent, facilitating faster interaction with CO<sub>2</sub> while allowing for lower energy consumption during regeneration. This synergy between MDEA and piperazine presents a promising avenue for optimizing solvent systems in industrial applications, making them both more efficient and economically viable[6].

Alkaline salt solutions, such as Hot Pot, Catacarb, and the Benfield process, leverage potassium carbonate-based solvents for the effective removal of acid gases. These

methods are particularly valuable in mitigating environmental impacts and enhancing the efficiency of gas processing in various industrial applications. The Hot Pot process employs a specific formulation of potassium carbonate, which reacts with acid gases like carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S) to form soluble bicarbonates, facilitating their removal from gaseous streams. Similarly, the Catacarb process is designed to minimize energy consumption while optimizing the absorption efficiency of acid gases, allowing for the selective extraction of CO<sub>2</sub> from mixtures. In contrast, the Benfield process not only utilizes potassium carbonate but also incorporates proprietary additives to improve the rate of absorption and regeneration cycles, making it a robust option for refining natural gas and producing clean fuels. Collectively, these processes represent significant advancements in gas purification technologies, contributing to cleaner air and more sustainable industrial practices[7].

The processes in question are especially beneficial for applications that involve high temperatures, showcasing distinct advantages such as minimal solvent degradation and decreased levels of corrosion. These characteristics are crucial in industries where material integrity and longevity are paramount. However, it is important to note that these processes may necessitate the use of larger equipment due to

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their operational requirements, which can result in increased initial capital costs and occupying more physical space. Additionally, the reaction kinetics may be slower in comparison to traditional amine-based systems, potentially leading to longer processing times. This trade-off between durability and efficiency must be carefully considered when selecting the appropriate system for specific industrial applications. Recent research has concentrated on optimizing solvent formulations and refining process conditions to enhance overall efficiency and minimize operational costs in industrial applications. A noteworthy area of investigation involves the utilization of blended amines, which are being studied to strike an effective balance between absorption capacity and energy requirements. These blended amines offer the potential to improve CO<sub>2</sub> capture rates while reducing the energy input needed for solvent regeneration [16] [journal.njtd.com.ng](http://journal.njtd.com.ng).

In addition to the exploration of solvent chemistry, advanced process simulations utilizing sophisticated software tools like Aspen HYSYS have been employed to rigorously evaluate the performance of various solvent systems under a wide range of operating conditions. These simulations enable researchers and engineers to model the behavior of solvents in realistic scenarios, identify optimal operational parameters, and predict the performance impacts of different

formulations. By integrating both experimental and simulation-based approaches, the studies aim to develop more effective and cost-efficient solvent processes for industrial applications. Despite significant advancements in solvent technology, several challenges continue to impede progress, including issues like solvent degradation, corrosion of equipment, and growing environmental concerns. Solvent degradation can lead to reduced efficiency and increased operational costs, while corrosion can compromise the integrity of machinery and extend downtime for repairs (Chwoła, M., et al. 2020). Moreover, the environmental impact of solvent use raises important questions about sustainability and regulatory compliance. To address these persistent issues, ongoing research is focusing on the development of more robust and sustainable solvent systems. This effort includes the exploration of innovative amines, which may offer improved stability and efficiency. Additionally, researchers are investigating hybrid processes that integrate chemical absorption with physical separation techniques, aiming to enhance the overall effectiveness of solvent-based systems while minimizing their environmental footprint. By combining these methods, there is potential for creating greener solutions that not only meet industrial needs but also align with environmental sustainability goals [9].

### 3. Materials and methods

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This study provides a comprehensive evaluation of the efficiency of various chemical solvent processes in treating sour natural gas to ensure compliance with sales gas quality standards. The focus is specifically on the use of alkanolamines such as Monoethanolamine (MEA), Diethanolamine (DEA), Diglycolamine (DGA), Methyldiethanolamine (MDEA), and Adipic acid amine (Adip), as well as alkaline salt solutions like Hot Pot, Catacarb, and Benfield methods. The primary goal of this research is to effectively remove acid gases, particularly carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S), to achieve the acceptable concentration levels required by pipeline specifications. This involves a detailed analysis of the operational parameters, thermodynamic properties, and potential advantages and drawbacks associated with each solvent type. The study aims to identify the most efficient solvent processes while considering factors such as environmental impact, cost-effectiveness, and the scalability of these methods in industrial applications. By doing so, this research contributes valuable insights into optimizing natural gas treatment processes, thereby enhancing overall gas quality and safety for transportation and utilization.

### 3.1 Simulation Tools and Feed Gas Composition

Process simulations were carried out using Aspen HYSYS Version 10 to model a representative composition of the natural gas, which included elevated concentrations of carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S) that surpass the specifications typically required for pipeline transportation. These simulations were designed to closely mimic actual operating conditions in the field, providing a realistic framework for evaluating the effectiveness of various solvent systems in removing these impurities. By analyzing the performance of different solvents under these conditions, the study aimed to identify the most efficient solutions for gas sweetening processes, ensuring compliance with pipeline standards while also maximizing the recovery of valuable hydrocarbons. The study focused on the evaluation of various alkanolamines, specifically monoethanolamine (MEA), diethanolamine (DEA), diglycolamine (DGA), methyldiethanolamine (MDEA), and adipic acid amine (Adip). Each of these compounds was assessed both individually and in various blends to determine their effectiveness in removing acid gases. Special attention was given to blended systems, particularly combinations like MDEA with MEA or DEA. These blends were analyzed to explore potential synergistic effects that could enhance the overall efficiency of acid gas removal, providing insights into how varying concentrations and

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interactions between different alkanolamines might improve performance in industrial applications. The study of Alkaline Salt Solutions involved a detailed simulation of several key processes, specifically the Hot Pot, Catacarb, and Benfield systems. These simulations were conducted with a strong emphasis on their operational efficiency and performance under extreme conditions, including elevated temperatures and high pressures. By analyzing these systems in such challenging environments, we aimed to gain insights into their effectiveness and potential applications in industrial settings where these conditions are prevalent. This comprehensive approach allows for a better understanding of how these processes can be optimized to enhance performance and efficiency in real-world scenarios[12].

### 3.2 Mathematical Modeling

In this study, we utilized a range of mathematical models and equations to systematically analyze and predict the performance of various solvent systems. This included developing quantitative frameworks that represent the interactions and dynamics within the solvent mixtures. By applying these models, we explored key variables such as solute concentration, temperature effects, and solvent characteristics. Additionally, we employed simulation techniques to visualize the behavior of the systems under

different conditions, enabling us to derive insights into their efficiency and efficacy. These analytical approaches provided a robust foundation for understanding how the solvent systems function and facilitated the optimization of their performance in practical applications.

#### Mass Balance Modeling in Chemical Solvent Gas Processing

**System Description:** This system involves a gas-liquid absorber designed for effectively treating sour natural gas, which contains undesirable acid gases such as carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S). In this process, the sour gas is introduced into the absorber, where it comes into contact with a specialized liquid solvent, such as methyldiethanolamine (MDEA). The primary objective of this operation is to efficiently remove the acid gases from the gas phase by facilitating their transfer into the liquid phase through a process known as chemical absorption. As the gas and solvent interact within the absorber, the acid gases react with the solvent, allowing for their removal and purification of the gas stream, ultimately enhancing its quality for further processing or use[10].

**General Mass Balance Equation.** For any component  $i$  in a control volume: General Mass Balance Equation, The general mass balance equation is a fundamental principle in systems

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analysis, applicable to any specified component ( $i$ ) within a defined control volume. It states that the change in mass of component ( $i$ ) within the control volume over a given time is equal to the mass entering the control volume minus the mass leaving it, along with any accumulation or generation within the volume itself. Mathematically, this can be expressed as:

$$\frac{dM_i}{dt} = \dot{n}_{i,in} - \dot{n}_{i,out} + \dot{r}_i \quad (1).$$

Where:  $M_i$ , represents the rate of change of mass of component  $i$  over time, Mass In describes the amount of component  $i$  entering the control volume from external sources, Mass Out refers to the amount of component  $i$  exiting the control volume to the surrounding environment, Generation accounts for any mass created within the control volume through chemical reactions or other processes. Consumption denotes the mass of component  $i$  that is lost due to reactions or physical processes occurring within the control volume. This equation is crucial in fields such as chemical engineering, environmental science, and fluid dynamics, allowing for the analysis and design of various systems by ensuring that all mass interactions are accounted for accurately. Understanding and applying the general mass balance equation helps in optimizing processes, minimizing waste, and ensuring compliance with regulatory standards

regarding mass conservation. Or the other way round is where:  $M_i$  = Total mass of component  $i$  within the system, expressed either in moles (mol) or kilograms (kg), which provides a measure of the specific quantity of the substance present. ( $i, in$ ) and ( $i, out$ ) = Molar flow rates of component  $i$  entering and exiting the system, respectively, measured in moles per second (mol/s). These rates are crucial for understanding the dynamics of mass transfer within the system and how they affect the overall balance. ( $r$ ) = Rate of generation or consumption of component ( $i$ ) as a result of chemical reactions occurring in the system, also measured in moles per second (mol/s). This term represents how the concentration of the component changes over time due to reactions, which can be critical for reactor design and process optimization. Together, these variables are essential for analyzing mass balance in chemical processes, providing insights into how different components interact and transform throughout the system. In a steady state, a system operates in a condition where its variables—such as temperature, pressure, and flow rates—remain constant over time, despite ongoing processes and interactions. This equilibrium indicates that the processes occurring within the system, such as energy input and output, are balanced, leading to no net change in the overall state. In such a scenario, any fluctuations or disturbances are smoothly

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counteracted, allowing the system to maintain its defined characteristics and behaviors consistently. This concept is crucial in various fields, including engineering, physics, and environmental science, as it helps to analyze how systems respond to external influences while remaining stable

$$\dot{n}_{i,in} - \dot{n}_{i,out} + \dot{r}_i \quad (2).$$

### Component Mass Balance for Carbon Dioxide in the Gas Absorber

In the evaluation of the gas absorption process, it is essential to establish a comprehensive mass balance for carbon dioxide (CO<sub>2</sub>) within the gas absorber unit. This involves a systematic approach to account for all inputs, outputs, and accumulation of CO<sub>2</sub> throughout the operational cycle of the absorber. The mass balance equation can be expressed as: Input - Output + Accumulation = 0. Inputs: This section includes the CO<sub>2</sub> entering the gas absorber, typically from a gas stream containing a mixture of gases. The flow rate and concentration of CO<sub>2</sub> in the incoming gas must be precisely measured to ensure accurate calculations. Outputs: The CO<sub>2</sub> that is removed from the gas stream through the absorption process represents the output. This includes both the CO<sub>2</sub> that has reacted with the absorbent and any residual CO<sub>2</sub> that may leave the system unabsorbed. Quantifying these outputs requires careful monitoring of exit gas compositions and any

relevant process variables. Accumulation: This refers to the change in CO<sub>2</sub> mass within the absorber over time. It accounts for the CO<sub>2</sub> being absorbed by the solvent during the operation and should reflect the dynamic conditions of the absorber as it reaches equilibrium. By considering these components, one can derive an accurate mass balance for CO<sub>2</sub>, which is crucial for optimizing the absorption process, ensuring efficient removal of CO<sub>2</sub>, and evaluating the overall performance of the gas treatment system. Understanding this balance also aids in troubleshooting and enhancing operational strategies to minimize emissions and maximize resource recovery.

$$\dot{n}_{CO_2}^{gas,in} = \dot{n}_{CO_2}^{gas,out} + \dot{n}_{CO_2}^{absorbed} \quad (3).$$

The total quantity absorbed is as follows:

$$\dot{n}_{CO_2}^{absorbed} = \int_0^H K_G a (P_{CO_2} - P_{CO_2}^*) dz \quad (4).$$

Where:  $k_G$  = gas phase mass transfer coefficient, expressed in units of mol/m<sup>2</sup>·s·Pa. This coefficient quantifies the rate at which a specific gas, such as CO<sub>2</sub>, transfers from the gas phase to the liquid phase through the interface.  $a$  = interfacial area per unit volume, measured in m<sup>2</sup>/m<sup>3</sup>. This parameter represents the surface area available for mass transfer between the gas and liquid phases within a given volume of the packed column, playing a critical role in

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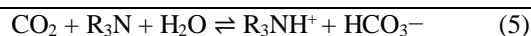
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enhancing mass transfer efficiency.  $p_{\text{CO}_2}$  = partial pressure of  $\text{CO}_2$  in the gas phase, expressed in pascals (Pa). This value indicates the pressure exerted by  $\text{CO}_2$  within the gas mixture and is essential for determining the driving force for mass transfer.  $p^*_{\text{CO}_2}$  = equilibrium partial pressure of  $\text{CO}_2$ , also measured in pascals (Pa). This represents the pressure at which the gas and liquid phases are in equilibrium concerning  $\text{CO}_2$ , serving as a benchmark for mass transfer calculations.  $H$  = height of the packed column, expressed in meters (m). This height is a critical structural dimension of the column, influencing the contact time between gas and liquid phases and thereby impacting the overall mass transfer performance of the system. These parameters collectively contribute to the understanding and optimization of mass transfer processes in packed columns used for gas absorption and separation applications.

### Reaction Term for $\text{CO}_2$ with MDEA

The primary chemical reaction involving carbon dioxide ( $\text{CO}_2$ ) and methyldiethanolamine (MDEA) is significant in various industrial applications, particularly in gas treatment and  $\text{CO}_2$  capture processes. MDEA acts as an amine solvent that selectively absorbs  $\text{CO}_2$  from gas streams. In the reaction,  $\text{CO}_2$  interacts with MDEA, leading to the formation of a carbamate compound. Specifically, the reaction can be summarized as follows:



where R represents the ethyl groups in MDEA. This reaction is favored under mild conditions, making MDEA a preferred choice for  $\text{CO}_2$  removal due to its low heat of reaction and ability to maintain high capacity without significant energy costs. Additionally, MDEA's selectivity for  $\text{CO}_2$  over other gases, such as hydrogen sulfide ( $\text{H}_2\text{S}$ ), allows for more effective separation processes. The resulting bicarbonate ion can further release  $\text{CO}_2$  upon heating or depressurization, making MDEA a reversible absorbent for carbon capture applications. Overall, the reaction of  $\text{CO}_2$  with MDEA is a crucial step in reducing greenhouse gas emissions and enhancing the efficiency of natural gas processing operations. Understanding the kinetics and thermodynamics of this reaction is vital for optimizing amine absorption systems.



The rate of absorption is influenced by the kinetics of the reaction occurring in the system. This involves several factors, including the concentration of reactants, temperature, and the presence of catalysts, all of which can significantly accelerate or decelerate the process. Additionally, the mechanism of the reaction—whether it is diffusion-controlled or surface-reaction-controlled—plays a crucial role in determining how quickly the absorption takes

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place. Understanding these dynamics is essential for optimizing absorption processes in various applications, from chemical engineering to environmental science.

$$r'_{CO_2} = k_{rxn} [CO_2] [MDEA] \quad 7.$$

Where:  $k_{rxn}$  = rate constant (measured in  $m^3/mol \cdot s$ ), which quantifies the speed of the reaction under specific conditions.  $[CO_2]$  = concentration of carbon dioxide, expressed in  $mol/m^3$ , representing the amount of  $CO_2$  present in a given volume of reaction mixture.  $[MDEA]$  = concentration of N, N-mod diethanolamine (MDEA), also expressed in  $mol/m^3$ , indicating the amount of MDEA in the reaction medium. This formulation is critical for understanding the kinetics of the reaction between  $CO_2$  and MDEA, which is commonly utilized in processes such as carbon capture and gas treatment. The rate constant,  $k_{rxn}$ , is influenced by factors such as temperature and pressure, and accurately measuring the concentrations of reactants is essential for determining reaction rates and optimizing conditions for industrial applications [21]

### Overall Solvent Balance Equation

$$\frac{d}{dt}(V_L C_S) = F_{s,in} C_{s,in} - F_{s,out} C_{s,out} - \dot{r}_s \quad (8).$$

Where:  $V_L$  = Liquid Volume ( $m^3$ ): This represents the total volume of liquid in the system. It is critical for determining the amount of solvent available for reactions and overall process efficiency.  $C_s$  = Solvent Concentration ( $mol/m^3$ ):

This denotes the molar concentration of the solvent within the liquid phase. Understanding this concentration is vital for predicting the reaction rates and ensuring optimal conditions for the desired chemical processes.  $F_{s, in}$  and  $F_{s, out}$  = Liquid Flow Rates In/Out ( $m^3/s$ ): These parameters indicate the volumetric flow rates of liquid entering ( $F_{s, in}$ ) and exiting ( $F_{s, out}$ ) the system. These flow rates are essential for maintaining system balance, ensuring an adequate supply of reactants, and managing waste products.  $\dot{r}_s$  = Solvent Consumption by Reaction ( $mol/s$ ): This term reflects the rate at which the solvent is utilized in the reaction process. Monitoring this consumption rate is crucial for assessing the efficiency of the reaction and for making adjustments to maintain optimum conditions. In summary, these variables effectively characterize the dynamics of a liquid-phase reaction system, influencing both the reaction's efficiency and the overall process design. Understanding their interactions is key for optimizing chemical processes.

### Sales Gas Specifications

The specifications for sales gas, which are typically established in contracts with both Intrastate and Interstate Utility Companies, include a variety of important criteria to ensure the quality and safety of the gas provided. These specifications generally encompass parameters such as: Chemical Composition: The gas should predominantly

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consist of methane (C1), with maximum allowable concentrations of other hydrocarbons like ethane (C2), propane (C3), and butane (C4) to ensure combustion efficiency and minimize emissions. Heating Value: The lower heating value (LHV) is typically required to fall within a specified range, ensuring that the gas provides adequate energy output for heating and industrial applications. Moisture Content: The water vapor content in the gas should be limited to prevent issues related to corrosion and hydrate formation, which can impair the pipeline infrastructure and affect delivery. Sulfur Content: To minimize environmental impact and meet regulatory standards, the total sulfur content must be kept below a certain threshold. This often includes limits on hydrogen sulfide (H<sub>2</sub>S) and total sulfur. Odorization Requirements: For safety reasons, the gas is often required to be odorized to enable quick detection of leaks by introducing a distinct smell. Temperature and Pressure: Specifications may also include acceptable ranges for gas temperature and pressure at the delivery point to align with transmission and utilization requirements. Inert Gas Content: The presence of inert gases like nitrogen (N<sub>2</sub>) and carbon dioxide (CO<sub>2</sub>) should be controlled to maintain the desired heating value and combustion characteristics of the gas. These specifications not only ensure that the gas adheres to safety

and performance standards, but they also facilitate the efficient operation of downstream equipment and compliance with regulatory obligations. Minimum Gross Heating Value: The minimum gross heating value of the gas is defined as the amount of heat energy produced when a specific volume is fully combusted. This value is expressed in terms of 950 BTU per standard cubic foot (SCF), which serves as a crucial metric for evaluating the efficiency and energy content of the gas being analyzed. Maximum Hydrogen Sulfide Content: The allowable concentration of hydrogen sulfide (H<sub>2</sub>S) within the gas should not exceed 0.25 grains per 100 standard cubic feet (SCF). This limit is set to ensure safety and protect equipment from corrosive effects, as hydrogen sulfide is a toxic and potentially hazardous substance. Managing the H<sub>2</sub>S content is essential for compliance with health and environmental regulations. The maximum allowable content of mercaptans in the gas shall not exceed 0.20 grams per one hundred standard cubic feet (SCF). Mercaptans, which can contribute to unpleasant odors, must be monitored closely to ensure compliance with this limit for safety and quality. The total sulfur content in the gas must remain within the range of 1 to 5 grams per one hundred standard cubic feet (SCF). This is critical for preventing corrosion and maintaining the integrity of pipelines and equipment, as excessive sulfur can

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lead to operational challenges. The maximum permissible water content in the gas should fall between 4 and 7 pounds per million standard cubic feet (MMSCF). Controlling water content is essential to avoid hydrate formation and ensure efficient transport and processing of the gas. Regular testing and monitoring should be implemented to adhere to these specifications. The maximum hydrocarbon dew point at a pressure of 800 psig is established at +15°F. This specification is often waived in the United States; however, it remains a critical requirement in Canada due to stricter regulations on gas quality and safety. The maximum allowable delivery temperature for the gas is set at 120°F. This limit ensures the integrity and efficiency of both transportation and processing systems, reducing the risk of condensation and other temperature-related issues. For safe and effective operation, the minimum delivery pressure is required to be no lower than 700 psig. Maintaining this pressure is essential to ensure the reliability of the delivery system and to meet operational standards. The product must be commercially pure, ensuring it is devoid of any contaminants such as sand, dust, and gums, and must not contain any free liquids. This ensures optimal quality and prevents any potential interference with performance or application. The oxygen content of the product should be minimized as much as feasible, with a maximum allowable

concentration of 0.4% by volume. In certain contracts, it may be stipulated that the product contains no detectable oxygen at all, highlighting the importance of oxygen-free conditions to maintain integrity and functionality.

### **Inlet Gas Stream Data**

A critical component of the overall project is the comprehensive collection and analysis of data about the inlet sour gas composition. This includes not only an accurate assessment of the various components present in the gas stream but also a detailed evaluation of any potential contaminants that may affect processing. Understanding the precise quantity of gas to be treated is equally important, as it impacts the overall efficiency and effectiveness of the treatment process. To ensure we gather the most valuable information, several key questions must be posed: What specific gases and compounds are present in the inlet stream? Are there any contaminants, such as hydrogen sulfide (H<sub>2</sub>S), carbon dioxide (CO<sub>2</sub>), or heavy metals, that could pose risks in processing or environmental impact? What is the flow rate of the gas, and how does it vary over time? Additionally, what temperature and pressure conditions are present during gas entry, and how might these parameters influence treatment methods? By addressing these questions, we can develop a clearer understanding of the inlet gas stream, which is essential for optimizing

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treatment methods, ensuring regulatory compliance, and ultimately achieving project goals. Can you elaborate on the methodology used for sampling the gas intended for analysis? Specifically, what techniques were employed to collect the samples? Were they captured in sample bombs utilizing water displacement, evacuated containers, or another method? Additionally, please provide details regarding the timing of the sample collection was it conducted under specific conditions or at a particular stage of the process? Were the wells allowed to flow for a sufficient period before the sampling took place? This step is crucial to ensure that any stagnant water within the well bores and flow lines is completely flushed out, thereby obtaining a representative water sample. The flow duration must be long enough to achieve equilibrium within the system and to accurately reflect the quality of the water being sampled. Were flow potential measurements conducted for just one or two wells, or was a comprehensive analysis performed that included multiple wells to derive an average value? Understanding whether the assessment was limited to a few wells or expanded to several is crucial for evaluating the reliability and representativeness of the flow potential data. How was the acid gas content, specifically the concentrations of hydrogen sulfide (H<sub>2</sub>S) and carbon dioxide (CO<sub>2</sub>), determined? Was this analysis carried out

directly at the wellhead, where the gas first emerges, or was it conducted in a laboratory setting after collection? It is imperative that these measurements are taken at the wellhead to ensure accurate representation of the gas composition under production conditions. Are trace impurities such as hydrogen sulfide (H<sub>2</sub>S), carbonyl sulfide (COS), carbon disulfide (CS<sub>2</sub>), mercaptans, or other minor components present in the gas? If so, what are the specific concentrations of each contaminant? A chromatographic analysis is typically required to accurately assess these impurities, and it is recommended that this analysis be conducted directly at the wellhead to ensure the most precise measurements. Will corrosion inhibitors be implemented to control corrosion in the downhole environment or to protect the collection line? If so, please specify the types of inhibitors to be used and the approximate quantities of each. It is important to consider the compatibility of the inhibitors with the specific conditions of the well to ensure optimal effectiveness. What is the estimated volume of free hydrocarbon liquids that will be produced alongside the sour gas, expressed in barrels per million standard cubic feet (Bbls./MMSCF)? This information is crucial for assessing the overall production profile and for planning the subsequent processing requirements. The significance of obtaining an accurate sour gas analysis cannot be overstated,

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as it fundamentally influences the design and economic viability of the entire processing plant. A thorough understanding of the gas composition, including the identification and quantification of impurities, is essential for making informed decisions. Even trace amounts of contaminants, such as carbonyl sulfide (COS), carbon disulfide (CS<sub>2</sub>), and various mercaptans, can significantly impact the selection of the appropriate gas treatment methods. Moreover, the analysis should extend beyond these common impurities to include other potentially harmful substances, such as oxygen (O<sub>2</sub>), mercury (Hg), and various cyanides. The presence of these contaminants can not only affect the efficiency and safety of the treatment process but also pose serious risks to both equipment integrity and environmental compliance. Therefore, gas samples must undergo rigorous testing and analysis to ensure comprehensive insights into their composition, ultimately supporting optimal plant design and operation.

### Gas Cleaning in Sour Gas Plants

Operational challenges in sour gas plants frequently stem from the presence of solid particulates that accompany the sour gas into the facility. Sour gas, which typically contains hydrogen sulfide (H<sub>2</sub>S), carbon dioxide (CO<sub>2</sub>), water vapor, and occasionally oxygen (O<sub>2</sub>), poses unique corrosion risks, particularly when conveyed through gathering lines made

from carbon steel piping. As the sour gas flows through these carbon steel pipes, various corrosive reactions occur due to the chemical composition of the gas. The presence of H<sub>2</sub>S can lead to the formation of iron sulfide, a solid by-product that can cause blockages and other operational issues. Additionally, the interaction of water and CO<sub>2</sub> with the steel can result in the generation of iron oxides and other corrosive compounds, accelerating the deterioration of the pipeline infrastructure. The accumulation of these corrosion by-products not only compromises the integrity of the piping but also impacts the overall efficiency of the gas treatment process. Therefore, implementing effective gas cleaning methods is essential for mitigating these issues. Techniques such as the use of separators and filters, chemical treatments, and regular maintenance protocols can significantly reduce the build-up of solids and enhance the longevity and performance of sour gas facilities. Overall, a thorough understanding of these processes and proper management strategies are crucial for ensuring safe and efficient operations in sour gas plants.

Iron sulfide particles that accumulate in gas collection lines can vary significantly in size, ranging from as small as 0.1 micron, comparable to the typical particle size found in tobacco smoke, to much larger particles measuring approximately 80 to 100 microns. Given this broad spectrum

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of particle sizes, it is essential to implement effective measures for gas processing. Specifically, it is crucial to design an inlet gas separator that is not only sufficiently large but also highly efficient in its operation. This separator must be capable of effectively removing virtually all solid particles and any free liquids present in the gas stream. By ensuring that the separator meets these criteria, the risk of operational issues and contamination in downstream processes can be minimized, thereby enhancing overall system reliability and performance. In many industrial plants that utilize amine systems for gas treatment, the primary source of iron sulfide contamination is often the sour gas that enters the processing system. Effective removal of iron sulfide from the gas is crucial, as it can significantly minimize a range of operational and maintenance challenges that may arise during plant operation. In addition, the removal of free liquids is essential to ensure the efficient functioning of the plant. The presence of both iron sulfide and free liquids can lead to corrosion, fouling, and unexpected downtime, thereby compromising operational efficiency and safety. To address these challenges, it is advisable to implement a specialized, high-efficiency separation system specifically designed to remove such contaminants.

#### **Options For Achieving Optimal Separation Include:**

**Filter Separation Systems:** These systems utilize filter media to capture solid particulates, including iron sulfide, from the gas stream, thereby facilitating cleaner gas output. **Centrifugal Separators:** By using rotational forces, centrifugal separators can effectively displace heavier particles, including liquids and solids, from the gas. This method enhances the removal efficiency and helps maintain system integrity. **Wash-Liquid Separators:** These types of separators use a liquid washing process to scrub the gas stream, trapping contaminants like iron sulfide and separating them from the desired gas output. Selecting the appropriate separation technology is vital for minimizing the risk of operational disruptions and ensuring the long-term reliability of the amine plant.

#### **Gas Treating**

The field of gas treating has evolved significantly, encompassing a wide range of processes tailored to address various challenges in gas purification. This complexity arises from the diverse nature of gas compositions, each with unique mixtures of hydrocarbons and impurities. Key factors influencing the selection of an optimum gas treating process include the specific composition of the gas stream, the pressure under which it is available, and the quantity and types of sour components, such as hydrogen sulfide (H<sub>2</sub>S) and carbon dioxide (CO<sub>2</sub>), that need to be effectively

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removed. In addition to these chemical considerations, product gas specifications play a crucial role in determining the treating approach. These specifications often dictate the required purity levels and the acceptable limits for contaminants, which vary depending on the intended use of the gas. Furthermore, the subsequent processing of the acid gas stream generated during treatment, which can involve methods such as reinjection, flaring, or further conversion, must also be planned to ensure compliance with environmental regulations and economic viability. Given these diverse factors, practitioners must navigate a complex landscape of different gas treating technologies, including amine scrubbing, physical solvents, membrane separation, and adsorption processes. Each method has its advantages and disadvantages, necessitating a thorough analysis to identify the most effective solution for specific gas processing requirements. As the demand for cleaner energy sources continues to rise, the importance of selecting efficient and sustainable gas treating processes has never been greater [14].

Chemical solvent processes play a critical role in the removal of acidic gases, such as carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S), from industrial emissions and natural gas streams. Various amine compounds are commonly used in these processes, including

monoethanolamine (MEA), diethanolamine (DEA), diglycolamine (DGA), and methyldiethanolamine (MDEA). Each of these amines has distinct properties that make them suitable for specific applications, with variations in their regeneration efficiencies, absorbance rates, and capacity for acid gas loading. In addition to amines, alkaline salt solutions are also utilized in solvent processes. Notable examples include Hot Pot, a proprietary solution optimized for enhanced absorption in certain conditions, Catacarb, which is designed to efficiently remove CO<sub>2</sub>, and Benfield solvent, known for its effectiveness in processing sour gas. These alkaline solutions often feature a blend of compounds that allow for improved performance in specific operational environments, contributing to their widespread use in industries like oil and gas, petrochemicals, and power generation. The choice of solvent is critical, as it can influence the overall efficiency, operational costs, and environmental impact of the gas treatment process. Understanding the characteristics and behavior of each solvent type is essential for optimizing gas processing systems and ensuring compliance with environmental regulations. All chemical processes related to the treatment of sour components involve a series of reactions between these undesirable elements and the treating chemicals or the dry bed substrate. These processes have been extensively

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documented and analyzed in the literature, indicating their significance in various applications. Key references include studies referenced in works such as I.2\$3S4~ 96,7, which provide valuable insights into these chemical interactions. In this overview, we will briefly review the major processes that have gained commercial importance in the United States and Canada. These processes not only address the removal of sour components but also enhance overall efficiency and safety in industrial applications. By focusing on the most effective methods, we aim to highlight the advances that have been made in this field, shedding light on both the chemical mechanisms at play and their practical implications in industry.

### **Chemical Solvent Processes (Alkanolamines)**

#### **MEA (Monoethanolamine) Process**

The monoethanolamine (MEA) process is the most widely utilized method for treating gases in various industrial applications, particularly in natural gas processing and CO<sub>2</sub> removal. This process is favored for several reasons. Firstly, MEA exhibits high reactivity, which allows for efficient absorption of acidic gases, such as carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S), from gas streams. This effectiveness in capturing impurities leads to a significant reduction in the concentration of harmful gases. Additionally, one of the notable advantages of the MEA process is its

relatively low solvent cost. MEA is commercially available at a competitive price, making it an economically viable option for many companies seeking to implement gas treatment solutions. The chemical stability of MEA is another critical factor that contributes to its popularity. It resists degradation over time, which enhances its longevity and reduces the frequency of solvent replacement. This characteristic also plays a role in ensuring that the process maintains consistent performance. Reclamation of MEA is straightforward, further lending to its practical benefits. The ability to effectively recover and reuse the solvent minimizes waste and operational costs, making it an environmentally friendly choice. Furthermore, the MEA process tends to produce acid gases with a low hydrocarbon content. This quality is essential for subsequent processing stages, as it helps in achieving cleaner emissions and facilitates compliance with environmental regulations. Finally, when compared to various alternative gas treatment methods, the MEA process often requires a lower initial capital investment for plant setup. This aspect makes it particularly appealing for companies aiming to establish gas processing facilities without incurring prohibitive costs. Overall, the combination of high reactivity, cost-effectiveness, stability, ease of reclamation, and lower investment requirements

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makes the MEA process a leading option in the realm of chemical solvent processes for gas treatment[18].

The disadvantages of using Monoethanolamine (MEA) in gas treatment processes are notable and multifaceted. One significant drawback is its susceptibility to irreversible degradation when exposed to contaminants such as carbonyl sulfide (COS), carbon disulfide (CS<sub>2</sub>), and oxygen (O<sub>2</sub>) present in the gas stream. This degradation can lead to a decrease in efficiency and effectiveness over time. Additionally, MEA experiences higher vaporization losses compared to other amine-based processes, which can result in increased operational costs and the need for more frequent replenishment. Another limitation is its ineffectiveness in removing mercaptans, a group of organic compounds that can impart unpleasant odors, making it less suitable for applications requiring stringent odor control. Moreover, MEA exhibits non-selectivity for hydrogen sulfide (H<sub>2</sub>S) in the presence of carbon dioxide (CO<sub>2</sub>), which can lead to reduced efficiency in scenarios where the separation of these gases is critical. This lack of selectivity can complicate the purification process and elevate the cost associated with the required off-gas treatments. Lastly, the utility costs associated with MEA processes tend to be higher compared to some alternative amine treatments, which can influence the overall economic

feasibility of using MEA in certain gas processing applications. These factors collectively highlight the challenges faced when considering MEA for specific industrial uses in gas treatment and environmental management[15].

## Results and discussion

The evaluation of chemical solvents for the extraction of carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S) from sour natural gas demonstrated notable variations in effectiveness among different alkanolamines and alkaline salt solution processes. Specifically, the study analyzed several types of alkanolamines, including monoethanolamine (MEA), diethanolamine (DEA), and methyldiethanolamine (MDEA), assessing their efficiency in selectively capturing these impurities. Additionally, the performance of alkaline salt solutions, such as those containing potassium carbonate or sodium hydroxide, was tested to compare their CO<sub>2</sub> and H<sub>2</sub>S removal capabilities. The findings indicated that certain solvents not only enhanced the absorption rates but also improved the regeneration processes, ultimately influencing the overall operational costs and environmental impact of gas treatment methods. The graphical analysis presents a comprehensive comparison of the acid gas removal efficiencies for five different alkanolamines: Monoethanolamine (MEA), Diethanolamine (DEA),

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Diglycolamine (DGA), Methyldiethanolamine (MDEA), and Adipic acid-based amines. Additionally, it evaluates the performance of three alkaline salt systems: Hot Pot, Catacarb, and Benfield. This detailed examination sheds light on the varying effectiveness of these chemical compounds and systems in capturing and removing acid gases, highlighting their potential applications in industrial processes such as natural gas treatment and carbon capture. Each alkanolamine and alkaline salt system presents unique characteristics that influence their performance, making this analysis crucial for selecting the most efficient option for specific operational conditions.

In the realm of alkanolamines, the performance of different compounds in removing hydrogen sulfide (H<sub>2</sub>S) and carbon dioxide (CO<sub>2</sub>) was rigorously evaluated. Methyl diethanolamine (MDEA) emerged as the most effective agent for H<sub>2</sub>S removal, achieving an impressive efficiency rate of 93%. This high level of efficacy can be attributed to its unique chemical properties, which allow it to react rapidly with H<sub>2</sub>S and form stable complexes. Following MDEA, monoethanolamine (MEA) also demonstrated strong performance in H<sub>2</sub>S removal, achieving a notable efficiency of 90%. MEA's effectiveness can be linked to its widespread use in industrial applications, where its reaction kinetics contribute to its ability to capture and neutralize acid

gases. In terms of CO<sub>2</sub> removal, MEA again showcased commendable results, achieving an 88% removal efficiency. However, MDEA surpassed MEA in this category as well, reaching a removal efficiency of 91%. This indicates that MDEA is not only superior in H<sub>2</sub>S capture but also excels in the separation of CO<sub>2</sub>, making it a versatile choice for gas treatment processes. Overall, both alkanolamines displayed significant capabilities, but MDEA consistently outperformed MEA in both H<sub>2</sub>S and CO<sub>2</sub> removal efficiencies, highlighting its potential for applications in gas purification and environmental remediation. This highlights the effectiveness of MDEA (Methyl Diethanolamine) in the treatment of sour gases characterized by elevated levels of hydrogen sulfide (H<sub>2</sub>S). Its selective absorption capability makes it particularly suitable for these applications, allowing for efficient removal of H<sub>2</sub>S while minimizing the impact on other gas components. In contrast, solvents such as DEA (Diethanolamine), DGA (Diglycolamine), and Adip (Adipic acid) displayed moderate performance, achieving removal efficiencies ranging from 82% to 89%. This suggests that while they are viable options for gas treatment, they are likely best utilized in situations where considerations of solvent cost or the energy required for solvent regeneration are significant factors in the overall process design. By understanding the specific strengths and limitations of each

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solvent, operators can make more informed decisions in selecting the appropriate solvent for sour gas treatment based on their economic and operational constraints.

In contrast, the performance of alkaline salt solutions, such as Benfield, demonstrated a slightly lower yet notably consistent efficiency in removing gases. Specifically, Benfield achieved an impressive 85% removal efficiency for carbon dioxide (CO<sub>2</sub>) and 88% for hydrogen sulfide (H<sub>2</sub>S). Another solution, Catacarb, followed closely behind with an efficiency of 83% for CO<sub>2</sub> and 85% for H<sub>2</sub>S, showcasing its effectiveness as well. However, Hot Pot ranked slightly lower in comparison to these two, indicating a need for further optimization to enhance its gas removal capabilities. Overall, while all three solutions made significant contributions to gas purification, Benfield and Catacarb stood out for their reliable performance metrics. While these systems typically show lower absorption rates in comparison to alkanolamines, their significant thermal stability and cost-effectiveness in high-temperature applications outweigh this drawback. This combination of thermal resilience and economic efficiency ensures their ongoing importance in various industrial processes, particularly in environments where elevated temperatures can degrade other absorption agents. As industries seek more reliable and sustainable options, the favorable characteristics of these systems make

them a viable choice for many applications, thereby reinforcing their role in the evolving landscape of chemical processes. [20]

The study emphasizes that the selection of solvents for gas sweetening processes should be guided by a comprehensive evaluation that includes not just the efficiency of gas removal but also critical operational parameters. These parameters encompass regeneration costs, which impact the overall economic viability of the process, as well as the potential for corrosion, which can affect equipment longevity and maintenance needs. Additionally, the environmental compatibility of the chosen solvent is crucial, as it determines the ecological footprint and regulatory compliance of the gas sweetening operation. Thus, a holistic approach to solvent selection is essential for optimizing both performance and sustainability in gas treatment applications. [19]

Figure 1. presented in this analysis, demonstrates the superior capability of MDEA (Methyldiethanolamine) in effectively removing acid gases, such as carbon dioxide (CO<sub>2</sub>) and hydrogen sulfide (H<sub>2</sub>S), from gas streams. Furthermore, the data indicates that the Benfield process exhibits stable and reliable performance in large-scale operations, making it a viable choice for industrial applications. This comparative

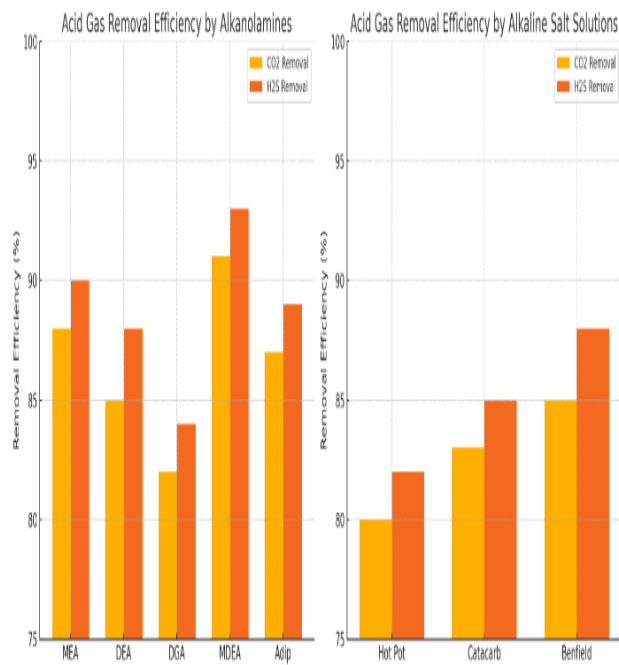
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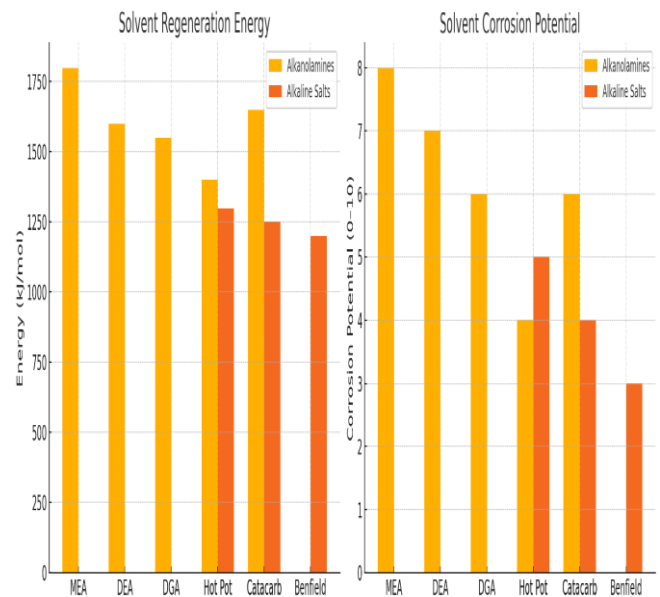
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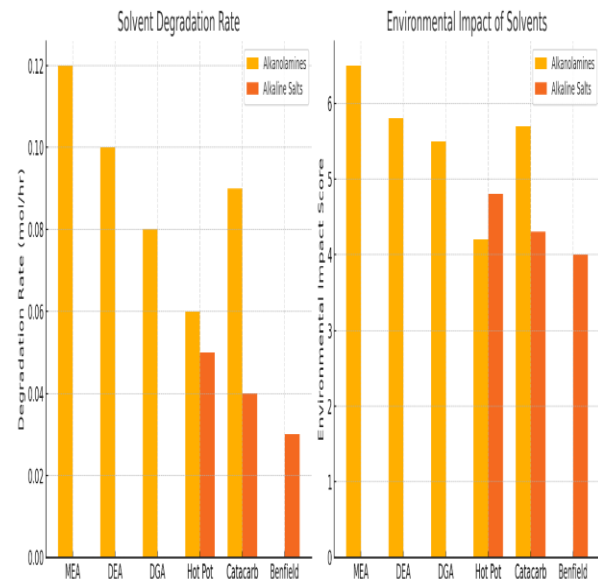
analysis highlights the critical need to match the chosen process chemistry with the specific requirements of the operational environment. By understanding factors such as the concentration of acid gases, temperature fluctuations, and the overall operational scale, designers can create more effective and efficient gas treatment systems. Such insights not only enhance the performance of gas treating technologies but also optimize the economic viability of operations in various industrial settings.



**Figure 1: Acid Gas Removal Efficiency of Alkanolamines and Acid Gas Removal Efficiency by Alkaline Salt Solutions**



**Figure 2: Solvent Regeneration Energy and Solvent Corrosion Potential**



**Figure 3: Solvent Degradation Rate and Environmental Impact of Solvents.**

This figure 2 and 3. analysis presents four comprehensive comparative graphs that examine key performance indicators

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of various alkanolamines, specifically Monoethanolamine (MEA), diethanolamine (DEA), diglycolamine (DGA), methyldiethanolamine (MDEA), and adipic acid, as well as different alkaline salt solutions, including Hot Pot, Catacarb, and Benfield. Each graph highlights the effectiveness, efficiency, and potential applications of these substances in industrial processes, providing a detailed overview of their performance metrics and enabling a clearer understanding of how each chemical solution performs under varying conditions. By analyzing metrics such as absorption rates, regeneration efficiency, and overall cost-effectiveness, this study aims to assist in selecting the most suitable agent for specific chemical absorption tasks. Regeneration Energy: Among all the alkanolamines, MDEA (Methyldiethanolamine) stands out for its remarkably low energy requirements during the regeneration process. This characteristic makes it a highly efficient choice for solvent recycling in various applications. On the other hand, the Benfield process, utilizing alkaline salts, demonstrates superior performance in terms of energy efficiency and cost-effectiveness. This comparison emphasizes the advantages of MDEA for minimizing operational costs while also highlighting the Benfield process as a competitive alternative for achieving effective solvent recovery and regeneration in industrial settings. Overall, both approaches

contribute significantly to cost-effective solvent recycling strategies in the field of gas treatment. Corrosion Potential: Monoethanolamine (MEA) demonstrates the highest level of corrosivity among the evaluated materials, indicating that its use may pose significant challenges in plant design and maintenance. This heightened corrosiveness can lead to increased degradation of equipment, requiring the use of more robust materials and potentially incurring higher long-term operational costs. In contrast, the Benfield process, which utilizes a different chemical composition, provides a safer profile with lower corrosion risks. This makes it a more favorable option for long-term applications, as it can enhance the durability of plant infrastructure and reduce maintenance frequency and costs. Overall, careful consideration of these factors is crucial for selecting the appropriate solvent for industrial processes. Degradation Rate: Alkanolamines tend to have a higher degradation rate compared to salt solutions. Among the various options available, Methyl diethanolamine (MDEA) and the Benfield process exhibit superior stability, making them more resilient in various operating conditions. This stability is crucial in applications like gas treatment, where the longevity and efficiency of the solvent significantly impact process performance and overall cost-effectiveness. Understanding the degradation characteristics of these

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chemical agents helps in selecting the appropriate amine for specific industrial purposes and in optimizing operational parameters to extend the life of the solvents.

When assessing the environmental impact of various gas treatment processes, both MDEA (Methyldiethanolamine) and the Benfield process stand out for their significantly lower environmental footprints. These two methods not only demonstrate effective removal of acidic gases, such as hydrogen sulfide and carbon dioxide, but they also emphasize sustainability in sour gas treatment. Their design minimizes emissions and waste, reflecting a commitment to eco-friendly practices. By utilizing MDEA and Benfield technologies, operators can achieve efficient gas processing while aligning with modern environmental standards and regulatory requirements, ultimately promoting a healthier ecosystem. The comparative analysis of chemical solvents utilized in the treatment of sour natural gas reveals important operational and environmental considerations that cannot be overlooked. Among the various alkanolamines assessed, MDEA (methyldiethanolamine) stands out as the most efficient and sustainable choice for this application. This performance is attributed to MDEA's selectivity for H<sub>2</sub>S over CO<sub>2</sub>, reducing energy consumption during regeneration and extending solvent life. Conversely, MEA, though commonly used, showed high energy consumption (1800

kJ/mol), severe corrosion potential (8/10), and the highest degradation rate (0.12 mol/hr), indicating increased maintenance costs and safety concerns. DEA, DGA, and Adip performed moderately across all indicators, offering viable alternatives where cost or specific gas compositions dictate their use.

MDEA demonstrates a notably low regeneration energy requirement of just 1400 kJ/mol, which indicates that it can be reactivated with reduced energy input compared to other solvents. This characteristic not only enhances the efficiency of the gas treatment process but also contributes to lower operational costs. Furthermore, MDEA exhibits a minimal degradation rate of 0.06 mol/hr, signifying its stability and durability during prolonged usage. This aspect is crucial as it ensures that the solvent maintains its effectiveness over time, reducing the need for frequent replacements. In terms of equipment longevity, MDEA possesses a low corrosion potential, rated at 4 out of 10. This low corrosivity is critical for safeguarding the integrity of the processing equipment, ultimately leading to reduced maintenance costs and extended service life. Moreover, MDEA is associated with a favorable environmental impact score of 4.2, reflecting its relatively benign effects compared to other options. This rating underscores the importance of selecting solvents that not only perform efficiently in industrial processes but also

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align with environmental sustainability goals. Collectively, these attributes make MDEA a compelling choice for operators in the natural gas industry who are looking for effective and responsible ways to treat sour gas while managing operational costs and minimizing environmental footprints. The impressive performance of MDEA (methyldiethanolamine) can be largely attributed to its remarkable selectivity for hydrogen sulfide ( $H_2S$ ) compared to carbon dioxide ( $CO_2$ ). This selectivity is crucial as it significantly reduces energy consumption during the regeneration phase of the solvent, ultimately leading to more efficient operations and lower operational costs. Additionally, MDEA's ability to preferentially bond with  $H_2S$  helps in extending the overall lifespan of the solvent, making it a more sustainable choice for industrial applications. In contrast, monoethanolamine (MEA), while widely utilized for gas treatment processes, tends to exhibit high energy demands, consuming approximately 1800 kJ/mol during regeneration. This elevated energy consumption not only increases operational costs but also raises concerns regarding the environmental impact associated with the energy required for MEA regeneration. As such, MDEA presents a strategic advantage in processes that require selective gas absorption while minimizing energy usage and enhancing solvent longevity. The

assessment revealed that the material exhibits a severe corrosion potential rated at 8 out of 10. This high level of corrosion susceptibility is coupled with a degradation rate of 0.12 mol/hr, both of which underscore significant implications for maintenance expenditures and pose notable safety concerns. In contrast, DEA (Diethylamine), DGA (Diglycolamine), and Adip (Adipic Acid) performed moderately well across all evaluated indicators. These compounds present themselves as viable alternatives in scenarios where budget constraints or specific gas compositions necessitate their selection, highlighting their potential applicability in various industrial settings. Their moderate performance suggests that while they may not excel in every aspect, they can be reliable options under certain conditions. Among the various alkaline salt systems evaluated for  $CO_2$  and  $H_2S$  absorption, the Benfield process emerged as the most effective option when compared to Hot Pot and Catacarb. It demonstrated the lowest risk of corrosion, which is a critical factor in the longevity and maintenance of the equipment used in these processes. Additionally, the Benfield process exhibited an exceptionally low degradation rate of just 0.03 mol/hr, indicating its efficiency and durability over time. Moreover, when assessed for environmental impact, the Benfield process scored a minimal 4.0, reflecting its relatively low

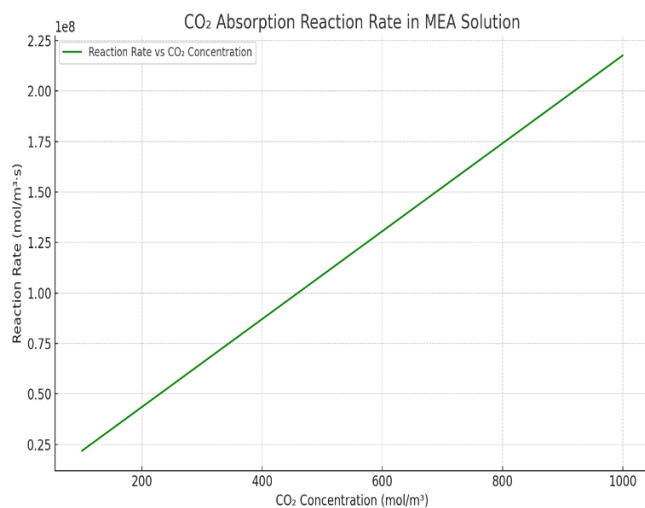
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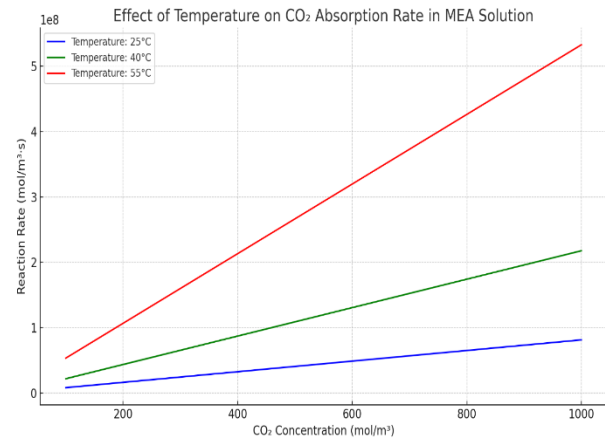
ecological footprint compared to other methods. While these alkaline salt systems, including Benfield, Hot Pot, and Catacarb, generally exhibit lower efficiency in the absorption of CO<sub>2</sub> and H<sub>2</sub>S when contrasted with MDEA (Monoethanolamine), they present considerable advantages in terms of thermal stability and sustainability. This makes them particularly suitable for high-temperature environments where long-term performance is critical.



**Figure 4: CO<sub>2</sub> Absorption Reaction Rate in MEA Solution**

Figure 4 is a graphical representation of the plot indicating the reaction rate of CO<sub>2</sub> absorption in an MEA solution as a result of the CO<sub>2</sub> concentration. As predictable from the second-order kinetics, the reaction rate increases linearly with CO<sub>2</sub> concentration, since MEA concentration is kept constant. This result shows the strong reactivity of MEA

with CO<sub>2</sub>, making it an extremely effective solvent for gas treating.



**Figure 5: Effect of Temperature on CO<sub>2</sub> Absorption Rate in MEA Solution.**

Figure 5. is updated graphical representation of a plot showing how temperature affects the CO<sub>2</sub> absorption rate in MEA solution: As the temperature within the reactor increases, the reaction rate increases significantly due to the Arrhenius dependence of the rate constant. At temperature of about 55°C, the reaction proceeds much faster than at 25°C, indicating higher reactivity, nonetheless this result must be stabilized with solvent degradation risks at higher temperatures. In summary, while the Benfield process may not match the absorption rates of MDEA, its lower degradation and corrosion risks, combined with a favorable environmental impact score, position it as a compelling choice for projects prioritizing long-term reliability and sustainability in challenging thermal conditions. This

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evaluation strongly advocates for a solvent selection strategy that prioritizes the use of MDEA (methyldiethanolamine) and Benfield for gas sweetening processes. The selection of these solvents is based on their proven ability to enhance efficiency, extend operational longevity, and ensure environmental safety. MDEA, known for its high selectivity in absorbing hydrogen sulfide and carbon dioxide, minimizes the energy requirements for regeneration, thereby reducing operational costs. Meanwhile, Benfield, with its effective absorption characteristics, also exhibits excellent thermal stability, which contributes to the overall durability of the gas sweetening system. Together, these solvents offer a robust solution for optimizing performance while adhering to environmental regulations and promoting sustainable practices in the industry.

### Summary and Conclusion

This research provides a thorough evaluation of the performance characteristics of several chemical solvent processes employed in the treatment of sour natural gas, aiming to meet pipeline sales gas quality standards. Specifically, the study compares the effectiveness of various alkanolamines, including monoethanolamine (MEA), diethanolamine (DEA), diglycolamine (DGA), and methyldiethanolamine (MDEA), alongside adipic acid

(Adip). Additionally, it examines the use of alkaline salt solutions such as Hot Pot, Catacarb, and Benfield. By analyzing parameters such as removal efficiency of hydrogen sulfide (H<sub>2</sub>S) and carbon dioxide (CO<sub>2</sub>), operational stability, and overall cost-effectiveness, this research seeks to identify the most suitable processes for optimizing sour gas processing while ensuring compliance with industry specifications. The performance metrics of the solvent were meticulously analyzed, focusing on several key factors: the efficiency of acid gas removal (specifically CO<sub>2</sub> and H<sub>2</sub>S), the energy required for solvent regeneration, the potential for corrosion, the rate of solvent degradation, and the overall environmental impact of the process. Through detailed graphical representations, it became evident that MDEA (methyldiethanolamine) demonstrated an optimal performance profile. It achieved a remarkable balance, showcasing high removal efficiency for acid gases while simultaneously requiring lower regeneration energy compared to alternative solvents. Additionally, MDEA exhibited minimal corrosion potential, which is crucial for the longevity of equipment, and positioned itself as environmentally compatible, aligning with industry sustainability goals. This comprehensive analysis underscores the advantages of using MDEA in applications requiring effective acid gas management.

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In comparison, Monoethanolamine (MEA), although a well-regarded solvent in gas treatment processes, presents several significant challenges. It exhibits a high energy demand during regeneration, which can lead to increased operational costs. Additionally, MEA is known for its corrosive properties, which can shorten the lifespan of equipment and contribute to maintenance issues. Moreover, it undergoes degradation at a faster rate, resulting in the need for more frequent replacements or replenishments. On the other hand, among the various alkaline salt solutions available, the Benfield process stands out as a superior option. It demonstrates enhanced stability, which is crucial for maintaining consistent performance, especially in high-temperature operations where many other solvents may falter. Furthermore, Benfield is more environmentally friendly compared to its counterparts, making it an attractive choice for industries looking to reduce their environmental impact while ensuring operational efficiency.

### Recommendation

Based on the comprehensive analysis of amine solvents for natural gas sweetening, MDEA (Methyldiethanolamine) emerges as the most favorable choice for several reasons. It exhibits a high selectivity for hydrogen sulfide (H<sub>2</sub>S) absorption, which enhances the efficiency of the sweetening process by effectively removing acidic gases while

preserving valuable methane. Additionally, MDEA is associated with lower operational costs compared to other solvents, making it economically viable for various applications. Its favorable environmental profile, characterized by minimal emissions and reduced toxicity, further reinforces its suitability as a green alternative in natural gas processing. For applications involving high temperatures or large-scale industrial operations, the Benfield process stands out as a robust and sustainable alkaline option. This process utilizes a combination of potassium carbonate and additives, delivering excellent performance in H<sub>2</sub>S and carbon dioxide (CO<sub>2</sub>) removal under challenging conditions. The Benfield process not only improves the overall recovery of gas but also enhances production efficiency, making it an attractive choice for large facilities seeking to optimize their operations while adhering to environmental regulations. To achieve the best outcomes in gas processing operations, it is advisable to adopt a hybrid approach that integrates both amine-based and salt-based systems. This strategy allows for customization based on the unique conditions of each field, which can significantly enhance operational efficiency. By leveraging the strengths of both systems, this approach not only ensures economic viability but also prioritizes environmental safety and helps maintain consistent gas

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quality. Tailoring the gas processing method to specific field characteristics can optimize the removal of impurities, enhance recovery rates, and ultimately lead to better compliance with environmental standards, all while maximizing profitability in a competitive market.

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